



## **BELTCON 4**

The Design of Belt and Apron Feeders at a Coal Mine

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## THE DESIGN OF BELT AND APRON FEEDERS AT A COAL MINE

### 1.0 SUMMARY

Operating conditions and client requirements require the use of large mass flow or expanded flow silos and bins in high capacity plants. Traditionally the load requirements of funnel flow bins and silos were less critical to material flow characteristics and accurate detail design, and some empirical formulae were used successfully. As the use of larger mass and expanded flow silos increased, the industry has learned quickly, mostly through bad experiences, that a more scientific approach to feeder and hopper design is essential.

### 2.0 INTRODUCTION

The object of this paper is to review

- a) the design of a high capacity belt feeder system presently in operation at Grooteegeluk I Coal Mine
- b) the design of apron feeders at the new Grooteegeluk II Coal Mine.

with emphasis placed on the design of a total integrated feeding system.

An attempt will be made to indicate the effect of factors, such as

- material characteristics,

- flow properties
- feed configurations, etc

on the design of feeders and a comparison of these designs to standard feeder calculations offered by suppliers in general to meet the requirements of a totally integrated system.

This paper is divided into two sections, namely

- a) The design and operation of large capacity coal belt feeders at Grootegeluk for feed of coal to the Matimba Power Station and
- b) The design of run-of-mine apron feeders for the new Grootegeluk II coal plant.

### 3.0 HIGH CAPACITY BELT FEEDER SYSTEM IN OPERATION TO FEED COAL TO MATIMBA POWER STATION

#### 3.1 BACKGROUND

Iscor appointed the Consulting Engineering firm of Lategan, Smith and van der Linde Incorporated in 1982 for the design of the Matimba Power Station materials handling plant at Grootegeluk Coal Mine consisting of

- a multiple plant stockyard feed system
- a complete belt filter plant

- a three stream stockyard, each stream to be serviced by a 32 m boom travelling, luffing and slewing combination stacker/reclaimer, with a total live stockpile capacity of 750 000 ton, with stockpile dewatering facilities and blending capabilities
- automatic sampling plants before stacking
- automatic assizing and sampling facilities after stockpiling incorporating two 500 ton surge bin facilities
- complete 3 525 tph to 4 500 tph conveying system

At the same time the above Consulting firm was appointed by Escom for the design and contract management of the materials handling facilities between the mining plant described above and the power station incorporating:

- an approximate 4 000 m long overland 3 525 tph conveyor
- an operating and emergency stockyard with ancilliary conveyors and a 500 ton surge bunker facility.

Refer to overall flowsheet G0075004.

### 3.2 ASSIZING PLANT DESCRIPTION

After the 750 000 ton stockpile facility (before the 4 000 m long 3 525 tph overland conveyor) an automatic assizing/sampling facility, two 500 ton surge bins were installed for the following reasons:

- to provide surge capacity between the combination stacker/reclaimer with an output varying between 2 000 tph and 5 500 tph and the overland conveyor which must be evenly fed at a maximum rate of 3 525 tph
- to provide adequate surge to the Mine for emptying the reclaim conveyor system in case the feed system to the power station is out of operation, thus ensuring continuous stacking flexibility and maintenance availability of the reclaim system on the Mine.
- as a fixed operational/maintenance takeover point between the Mine and Escom.
- as a facility of payment/takeover between the two parties based on assized quantity and quality.

The plant consists of

- a) a 2 100 mm wide feed conveyor
- b) an automatic proportioning gate for feed to either of the two 500 ton bins

- c) two 500 ton rectangular steel mass flow bins, with hopper angles at  $21^{\circ}$  and  $16,4^{\circ}$  to the vertical and lined with stainless steel SS304 liners. Each bin is provided with a belt feeder on the discharge and the complete system is supported on six 100 ton assizeable load cells. One bin is used for assizing purposes whilst the other bin is used as a surge facility only. The assized bin is provided with an automatic mass loading facility by means of 1 ton assized masses for calibration of the bin to its maximum capacity.

Signals from the load cells are used to

- control the feed out rate or
- to control the average reclaimer rate
- swing over the feed proportioning chute from the operating bin to the standby bin in case a high level is reached on the operating bin

- d) An automatic sampling plant, operating on time or mass base for

- moisture
- physical
- chemical

analyses for samples to all parties involved.

Refer to layout and plant flow flowsheets G0076309, G0076937, G0076930. G0076933 and G0077794.

### 3.3 COAL DATA

Coal to be handled was analysed and tested to define the following properties:

Size:	: 35 mm
Total moisture content	: 5% to 18.4%
Bulk density	: 850 kg/m <sup>3</sup> to 980 kg/m <sup>3</sup> dry
Angle of repose	: 38° to 45°
Angle of withdrawal	: 45° to 52°

Angle of friction of coal to stainless steel SS304:

Moisture	Angle $\phi$
18,4%	27°
13,4%	24°
7,95%	29° to 34°

Effective angle of internal friction  $\delta$

Moisture	Consolidated	$\delta$
14%	0	6°
14%	4,8 kPa	5°

Hopper side wall angle:  $\alpha = 21^\circ$

Hopper end wall angle :  $\theta = 16,4^\circ$

The latter information was obtained from Jenike and Johansen, who were responsible for testing of the material flow properties of the coal.

### 3.4 BIN CONFIGURATION AND VERTICAL FEEDER LOADS

Due to the large percentage of fines in the material (70% minus 6 mm), the high moisture content and for assizing purposes, the bins must be totally self emptying, thus dictating a mass flow design for the bin and hopper.

For a meaningful design it is important to be able to determine with reasonable accuracy the loads acting on the bin, bin hopper and the feeder and the corresponding power requirements.

The majority of formulae published are empirical in nature and derived to predict loads and power requirements for feeders used in conjunction with funnel flow bins. These formulae are inadequate when applied to massflow bins, as the load and power requirements are often greatly underestimated.

This is largely due to the fact that in mass flow bins the full area of the hopper outlet is presented to the feeder.

The loads acting on feeders and corresponding power requirements are influenced by several factors. These include the following:

- Flow properties of the bulk solid
- The actual hopper geometry
- The wall friction characteristics between the bulk solid and hopper/skirt walls
- Hopper flow pattern, whether mass flow, funnel flow or expanded flow.
- The chosen hopper shape, i.e. axi-symmetric, conical or a combination.
- The type of feeder and its geometry
- The initial filling conditions when the bin is filled from the empty condition and the flow condition when discharge has occurred.
- Super-imposed loading conditions on the feed material.
- Relative deflection between the bin/hopper and feeder under varying load conditions.

For a given bulk solid and hopper/feeder geometry, the load acting on a feeder varies considerably between the initial load, when the bin is first filled, and the load either during flow or after flow has stopped.

The method and procedure for estimating hopper and feeder loads has been established and viewed by A.W. Jenike, J.R. Johansen, A.W. Roberts, P.C. Arnold, A.G. MacLean and others. Using the above reference methods the vertical forces can be calculated.

### 3.4.1 Initial load condition

The normal wall pressure  $P_n$  is given by the Janssen equation:

$$P_n = \text{Bin pressure plus initial surcharge pressure}$$

$$= \frac{\gamma R}{\mu} (1 - e^{-\mu K_j h/R}) + P_{no} e^{-\mu K_j h/R}$$

$$\text{and } K_j = P_n / P_v$$

$$\text{and } P_{no} = K_j \gamma h_s$$

thus

$$P_v = \frac{Q_c}{A_c} = \frac{P_n}{K_j} = \frac{\gamma R}{\mu K_j} (1 - e^{-\mu K_j h/R}) + \gamma h_s e^{-\mu K_j h/R}$$

where

- $P_n$  = normal wall pressure
- $P_v$  = average vertical pressure
- $R$  = hydraulic radius
- $\mu$  = coefficient of wall friction =  $\tan$
- $h$  = bin height
- $h_s$  = effective surcharge
- $h_s = \frac{H_s}{m + 2}$

- $m = 0$  for triangular surcharge  
 $m = 1$  conical surcharge  
 $H_s =$  surcharge height  
 $K_j = P_n/P_v$   
 $= 0,4$  for slight convergences or  
 $= \frac{1 - \sin \delta}{1 + \sin \delta}$  with no convergences  
 $Q_c =$  Surcharge force at transition  
 $A_c =$  area at transition

For the bin and hopper geometry and factors as per section 3.3.  $Q_c/A_c$  varies from 51,69 kPa to 79,38 kPa.

To determine the load on the feeder an initial non-dimensional surcharge factor  $q_i$  can be calculated, i.e.

$$q_i = \left( \frac{\pi}{2} \right)^m \frac{1}{2(m+1) \tan \alpha} \left[ \frac{D}{B} + \frac{2Q_c \tan \alpha}{A_c \gamma D} - 1 \right]$$

- Where  $m = 0$  for plane flow  
 $m = 1$  for axi-symmetric flow  
 $B =$  hopper opening width  
 $D =$  bin width

and the total initial belt feeder vertical load  $Q_i$  is equal to

$$Q_i = q_i \gamma L B^2 \quad (\text{kN})$$

where  $L =$  hopper opening length

For the different factors and hopper outlet geometry the calculated results are as follows:

$$\begin{aligned}
 Q_{i \max} &= 440,5 \text{ kN with } q_i = 8,537 \\
 Q_{i \min} &= 342,4 \text{ kN with } q_i = 8,357
 \end{aligned}$$

### 3.4.2 Flow conditions

In the flow condition where the vertical support is removed, the major principal pressure acts more in the horizontal direction in the arched stress field above the feeder. Theoretical calculation for establishing the non-dimensional flow factor  $q_f$  are as follows:

$$\beta = \frac{1}{2} (\phi + \sin^{-1} \frac{\sin \phi}{\sin \delta})$$

$$X = \frac{2^m \sin \delta (\sin (2\beta + \alpha) + 1)}{1 - \sin \delta (\sin \alpha)}$$

$$Y = \frac{[2 (1 - \cos(\beta + \alpha))]^m (\beta + \alpha)^{1-m} \sin \alpha + \sin \beta \sin^{1+m}(\beta + \alpha)}{(1 - \sin \delta) \sin^{2+m}(\beta + \alpha)}$$

and

$$q_f = \frac{1}{4} (\pi/3)^m \frac{1}{\tan \alpha} \left[ \frac{Y (1 + \sin \delta \cos 2\beta)}{X-1 (\sin \alpha)} \right] \frac{1}{(\tan \alpha + \tan \theta - 1+m)}$$

and

$$Q_f = q_f \gamma L B^2 \text{ kN}$$

The calculated values for  $Q_f$  are as follows:

$$Q_f \text{ max} = 64,99 \text{ kN}$$

$$Q_f \text{ min} = 36,096 \text{ kN}$$

3.4.3 Comparison of theoretical and empirical calculations

Empirical formulae used for comparison are as follows:

- **Reisner's Method**

$$\frac{T_w}{\gamma B} = \frac{Y(1 + \sin \delta \cos 2\theta)}{2(X - 1) \sin}$$

and

$$\begin{aligned} Q_f &= T_w \times \text{hopper outlet area} \\ &= T_w \times L \times B \end{aligned}$$

- **Bruff's Method**

$$Q = \frac{2L^2 B^2 \gamma}{L + B} N_s \quad \begin{array}{l} \text{(slotted outlet including end)} \\ \text{(effects)} \end{array}$$

Where  $N_s = 4$  for initial filling condition

$N_s = 1$  for flow conditions

- **Johanson's Method**

$$Q_f = \gamma L B^2$$

#### 3.4.4 Jenike and Johansen

Jenike and Johansen use the non-dimensional  $q$  factor for the initial and flow conditions as calculated and multiplied by the mean outlet area and a dimensionless factor which depends on the loading condition, surcharge loads and method of feeder support to determine the total shear load.

A comparison between the empirical and theoretical calculations for the belt feeder are as follows:

Initial filling condition (filled from empty, inelastic support)

Method:	VERTICAL FORCE	
	$Q_i$ (kN)	
	Maximum	Minimum
Theoretical calculation	440,50	342,40
Bruff method	338,40	268,72
Jenike and Johansens method	546,79	424,84
Reisner	181,64	109,24

Flow conditions:

	VERTICAL FORCE	
	Qf (kN)	
	Maximum	Minimum
Theoretical	64,99	36,096
Reisner's method	45,41	27,31
Bruff's method	84,60	67,18
Johanson's method	51,60	40,98
Jenike and Johansen	65,66	37,19

3.4.5 Shear load due to vertical loads

The shear load acting on the belt feeder

$$Q_s = \mu Q$$

where  $\mu = \sin \delta$

In the initial filling condition

$$Q_{si} = \sin \delta Q_i$$

and for flow conditions

$$Q_{sf} = \sin \delta Q_f$$

However, due to the fact that stainless steel SS304 liners were installed on the outlet as well as the fact that a profiled outlet were installed (also to ensure even withdrawal of coal from the bin - refer to drawing G0076981) it was recommended by Jenike and Johansen to use  $\mu = 0,391$  and  $\mu = 0,796$  for initial and flow conditions respectively.

The resulting material shear loads, are then

$$Q_{si} = 213,951 \text{ kN}$$

$$Q_{sf} = 52,292 \text{ kN}$$

#### 3.4.6 Skirt plate friction

Skirt plate friction will occur in 2 areas, namely

- a) Skirt plates under the hopper which will be exposed to the bin vertical force

then

$$F_{skh} = \mu_2 K_v (2Q + \rho g B L y) y / B$$

and

- b) Skirt plates outside the hopper area where

$$F_{ske} = \mu_2 K_v \rho g (L_s - L) y^2$$

where

- $\mu_2$  = skirt plate friction co-efficient  
 $K_v$  = 0,4  
 $B$  = width between skirt plates  
 $L$  = skirt length under hopper

$L_s$  = total skirt length  
 $\rho$  = bulk density  
 $Q$  = initial filling or flow force  
under hopper  
 $y$  = average height of material  
against skirt plates

The calculated values of the total skirt plate friction are as follows:

Initial filling:

$$\begin{aligned} F_{si} &= F_{skh} + F_{ske} \\ &= 23,78 + 0,489 \\ &= 24,269 \text{ kN} \end{aligned}$$

Flow condition:

$$\begin{aligned} F_{sf} &= F_{skh} + F_{ski} \\ &= 3,24 + 0,328 \\ &= 3,568 \text{ kN} \end{aligned}$$

#### 3.4.7 Conveyor forces

Conveyor forces were calculated according to ISO 5048 and resulted in an additional load of 33,979 kN for conveying the material, special and secondary forces as defined.

#### 3.4.8 Total belt feeder forces

Total belt feeder forces  $T_e$  is equal to

- Shear load out of hopper plus

- Total skirt plate friction, plus
- Conveyor forces

and resulted in an initial horizontal load of 272,199 kN and a horizontal load under flow conditions of 89,839 kN.

### 3.5 DESCRIPTION OF BELT FEEDERS

The belt feeders are as outlined in drawing G0076302.

#### 3.5.1 General

The belt feeders are hydraulically driven, each capable of delivering coal at a rate of between 760 tph and 3 800 tph to the power station. Each belt feeder has 7 410 mm pulley centres, equipped with a 3 000 mm wide fabric belt and operating between 0,15 m/s and 0,75 m/s. Each conveyor is provided with a special screw take-up with a 1 000 mm travel and adjustment by hydraulic jack.

#### 3.5.2 Hopper and skirt plates

The feed hopper outlet commenced with a width of 600 mm at the back and tapers open to 1 040 mm at the outlet. Vertically the hopper outlet starts at 25 mm above the belt line and is profiled to a final bed depth of 785mm at the outlet. The complete hopper outlet is lined with 20 mm thick SS304 stainless steel liners. The shear plow at the hopper outlet is constructed in 27% high carbon chrome casting.

The skirt plates are 6 539 mm long, tapered from 2 000 mm inside steel at the back to 2 300 mm wide inside steel at the centreline of the head pulley. is 390 mm high and is lined with 20 mm thick stainless steel liners.

To the outside of the steel skirt plate a rubber skirt is installed to prevent spillage of fine coal in case of a wash down in the bin due to the high moisture content in the coal.

### 3.5.3 Belting

A 3 000 mm wide belt (two 1 500 mm wide belt longitudinally spliced together) were used with a maximum operating tension of 584 kN in the belt. The belt is a fabric belt, 6 ply, with 25 mm top cover and 5 mm bottom cover class 2500.

### 3.5.4 Pulleys

Pulleys are 1 400 mm diameter, lagged with 3 980 mm bearing centres and 380 mm bearing shaft diameter.

### 3.5.5 Idlers

Each set of idlers consists of 3 flat in-line rolls with a 20° trough idler at each end. Troughing idler spacing is at 480 mm centres and two of these idler sets were used on the return side installed invertedly for training. Each idler frame is installed on stools at both sides for removal by overhead crawl. The total load per idler amounted to 55,3 kN and a special design for the 675 mm face width idler was required. The roll diameter of the idler was selected as 230 mm, with an 80 mm shaft fitted with spherical roller bearings.

### 3.5.6 Drive

The required power and torque for the drive was as follows:

For normal running:

$$\begin{aligned}\text{Power} &= 89,839 \times 0,75 \text{ m/s} \\ &= 67,38 \text{ kW}\end{aligned}$$

$$\begin{aligned}\text{Torque requirements} &= 89,839 \times 0,707 \\ &= 63516 \text{ Nm}\end{aligned}$$

For start-up based on a belt speed of 0,2 m/s

$$\begin{aligned}\text{Power} &= 272,19 \times 0,2 \\ &= 54,438 \text{ kW}\end{aligned}$$

$$\begin{aligned}\text{Torque} &= 272,19 \times 0,707 \\ &= 192438 \text{ Nm}\end{aligned}$$

If an electrical drive were selected an equivalent motor size of

$$\frac{63516 \times 1500}{95 \times 9550} = 105 \text{ kW for normal running}$$

and

$$\frac{192438 \times 1500}{95 \times 9550 \times 1,4} = 227 \text{ kW for start-up}$$

A 95:1 reduction ratio and 1,4 start-up factor was required. Because of the torque requirements, and based on prices obtained for variable electrical drives and hydraulic drives, it was decided to use hydraulic system for each drive. Two power packs, each consisting of 4 x 45 kW drives (identical to power packs already available on the Mine) were used. A single Flender hydraulic motor with a planetary drive, torque arm mounted on each belt feeder and operating at a maximum pressure of 14,5 mPa is used.

Facilities are provided for reducing the number of power packs once the belt feeder is started-up and feeding at a constant rate.

### 3.6 RESULTS

After operation of approximately 18 months no problems were experienced on site with the belt feeders. Initial measurements indicated that power and torque requirements were within 70 to 90% of the calculated design values for normal running condition. Measurement of the values for the initial condition is obviously very difficult if not impossible.

## 4.0 DESIGN OF SILO APRON FEEDERS AT NEW GROOTEGELUK II COAL PLANT

### 4.1 INTRODUCTION

In this section the importance of material tests and proper designs based on the test results will be illustrated by means of practical examples as experienced on this mine.

At the present plant three series of silo systems are currently in use, of which the design was based on material test results. One of these systems is operating successfully. The other two systems were designed with an interface between two contractors at the silo hopper outlets, and not as integrated systems. These two systems do not operate satisfactorily in spite of the fact that funnel flow silos are used with relatively low feeder loads. The drives and the feeders proved to be incapable of handling the required loads, and spile bars are permanently installed in selective areas to allow operation.

Due to the above experiences the client was easily convinced that material tests and an integrated designed system was required for the following reasons:

- Prevention of failure of silos and hoppers due to collapsing of unstable arches after ratholing as experienced on the same plant.
- Proper operation of adequately sized hopper and feeder configurations.
- To ensure the most practical and economical design for the silos, hoppers and feeders in determining the type of silo, i.e. mass flow, funnel flow or expanded flow, as well as the type of feeder to be used.

## 4.2 BACKGROUND

Material is fed from the mine through a rotary breaker plant, breaking the coal to -150 mm and discarding the waste lumps. The material is then screened at 25/35 mm before being fed into the heavy medium cyclone and vessel plant storage silos. The screen oversize material is stored in three 4 000 ton silos before being fed to the heavy medium vessel plant, and the undersize is stored in five 2 000 ton silos before feeding the heavy medium cyclone plant.

## 4.3 DESIGN

### 4.3.1 Introduction

The material flow properties, hopper angles and wall loads were determined by Jenike and Johansen. The preliminary test results were used to execute feasibility studies regarding the silo and feeder types and define the design requirements of the feeders, based also on the experience on the other feeders.

### 4.3.2 Silo Configuration

Expanded flow silos were selected above mass flow silos on cost, while funnel flow silos were rejected due to the increased material segregation.

Although the client initially envisaged apron feeders underneath the vessel plant silos, and belt feeders underneath the cyclone plant silos, the high calculated feeder loads proved the belt feeders more costly, and apron feeders were used in both cases, which illustrates the importance of preliminary design in finalising the concepts.

#### 4.3.3 Feeder Selection

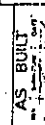
A comparison of the feeder loads, calculated as in section 3, with that of some of the tenderers who wished to ignore the specified loads, is given in the table below:

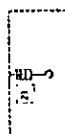
COMPARISON OF TOTAL HORIZONTAL FEEDER LOADS				
	GROUP 1 SILOS		GROUP 2 SILOS	
CONDITION	INITIAL (kN)	FLOW (kN)	INITIAL (kN)	FLOW (kN)
Specified Loads	451	132	300	86
Tenderer A	153	183	107	104
Tenderer B	169	112	114	76
Tenderer C	301	109	288	53
Tenderer D	62	55	56	16

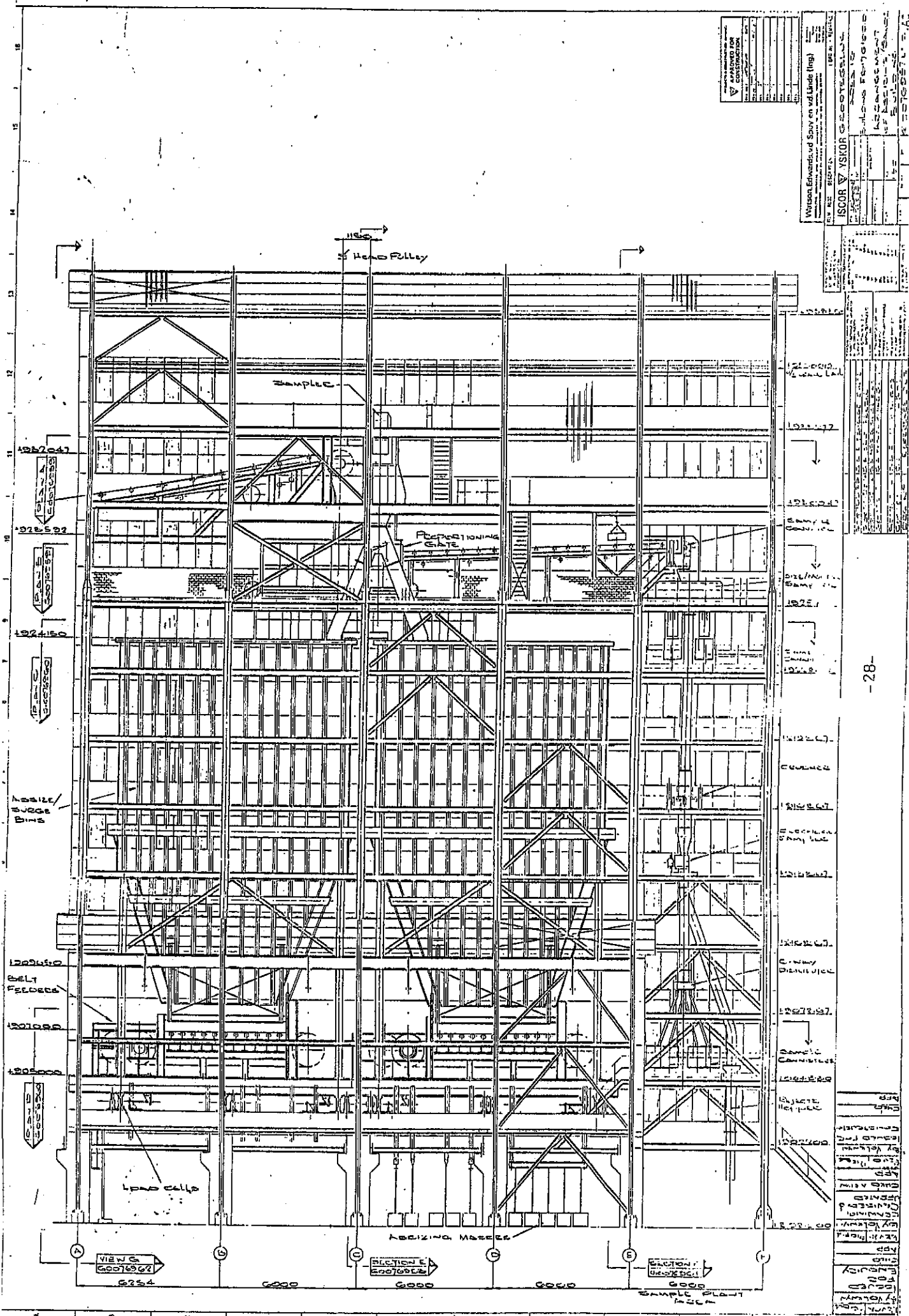
The same sizes and capacities for these feeders, as well as drawings of the silo and hopper configurations were given to all the tenderers. The loads given by the tenderers were based on their own methods of calculation, using empirical formulae ignoring flow conditions, hopper geometry and surcharge pressures. The variance in these results indicates the high risk inherent in empirical feeder design methods which would appear to relate to only specific operating situations but applied on a general basis. Should the end user of the equipment be solely motivated to select on the basis of lowest capital cost and validity of any guarantee, it is likely that he will select a feeder which will not do the duty.

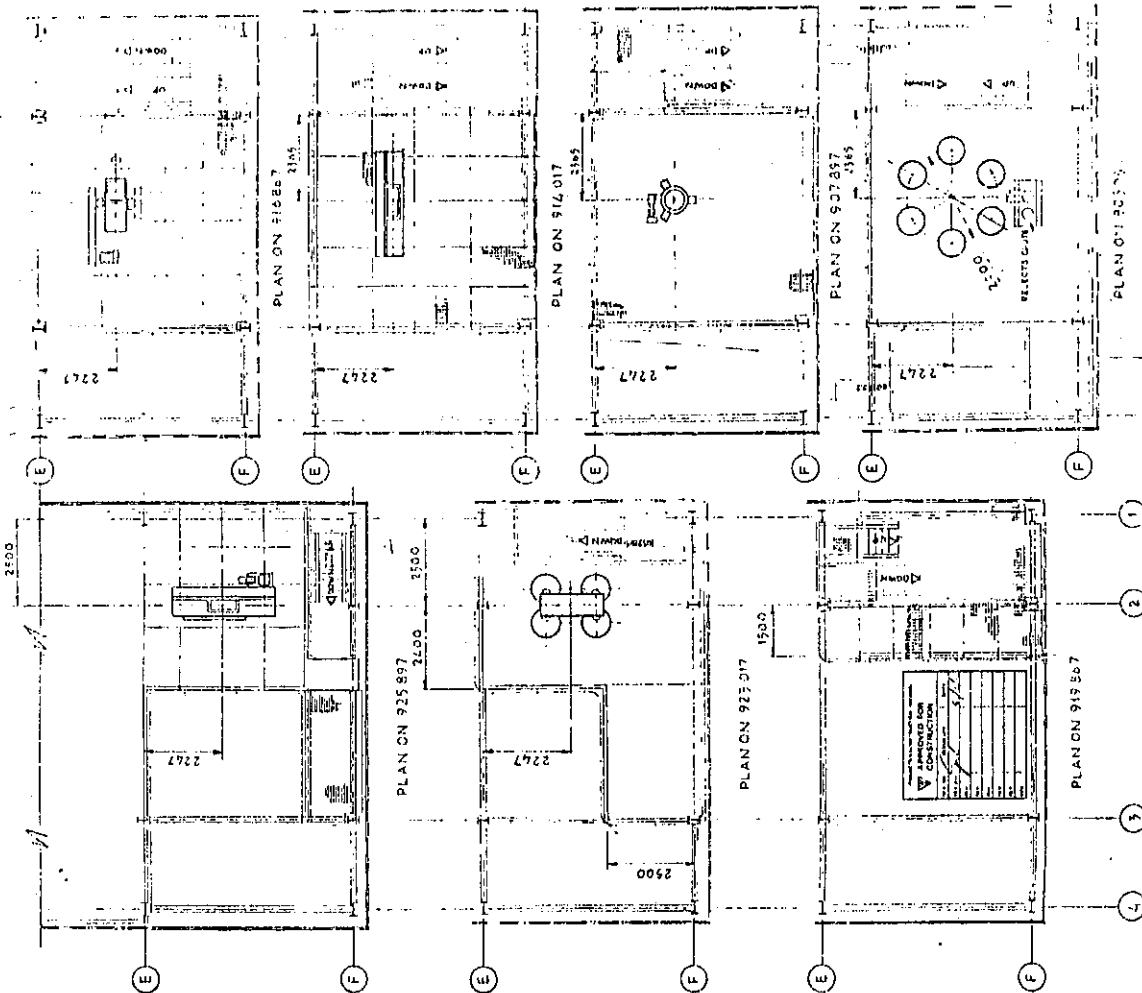
After detailed discussions with the tenderers, their offers were revised to comply with the specified loads, which were accepted by them in most cases.





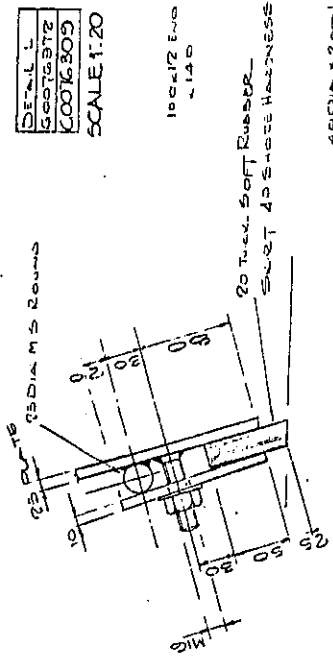
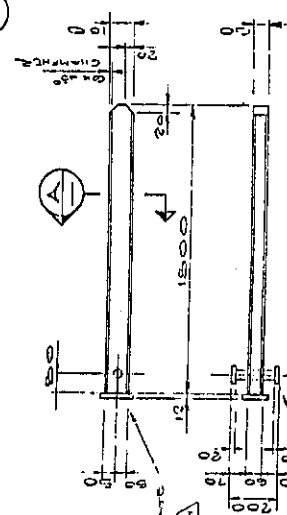
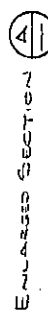






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1. PLATEWORK TO BE OF WELDED CONSTRUCTION  
6 mm CONTIGUOUS FILLET WELD UGS
2. 1/2" UGS THICKNESS AND MATERIAL TO BE AS  
PROJECT SPECIFICATION
3. ALL CHANNELS TO INSIDE OF PLATE UGS
4. FLANGES TO BE UGS
5. STIFFENERS TO BE PLAT UGS
6. SUPPORT BRACKETS FROM PLATE UGS
7. ALL BOLTS TO BE 1/2" FOR NOD BOLTING  
STANDARD UGS
8. LENGTH OF BOLTED HOLES DIMENSIONED AS  
SHOWN TO BE FULL LENGTH OF RUN
9. ERECTION BOLTS NUTS AND WASHERS TO BE  
AS SHOWN TO BE FULL LENGTH OF RUN  
CLEARLY WITH THE ASSEMBLY MARKINGS
10. FABRICATION TO SUPPLY TWO SETS OF ALL  
SHOP DETAIL DRAWINGS WITH ERECTION  
MATERIAL TO BE FOR APPROVAL  
PRIOR TO FABRICATION.
11. ERECTION MATERIAL TO BE  
AS SHOWN TO BE FULL LENGTH OF RUN

AS BUILT			
REV	DESCRIPTION	DATE	
02	Revised	8/2/86	

[illegible]

Year	1974	1975	1976	1977	1978	1979	1980	1981	1982	1983	1984	1985	1986	1987	1988	1989	1990	1991	1992	1993	1994	1995	1996	1997	1998	1999	2000	2001	2002	2003	2004	2005	2006	2007	2008	2009	2010	2011	2012	2013	2014	2015	2016	2017	2018	2019	2020	2021	2022	2023	2024	2025	2026	2027	2028	2029	2030	2031	2032	2033	2034	2035	2036	2037	2038	2039	2040	2041	2042	2043	2044	2045	2046	2047	2048	2049	2050	2051	2052	2053	2054	2055	2056	2057	2058	2059	2060	2061	2062	2063	2064	2065	2066	2067	2068	2069	2070	2071	2072	2073	2074	2075	2076	2077	2078	2079	2080	2081	2082	2083	2084	2085	2086	2087	2088	2089	2090	2091	2092	2093	2094	2095	2096	2097	2098	2099	2100
1974	1975	1976	1977	1978	1979	1980	1981	1982	1983	1984	1985	1986	1987	1988	1989	1990	1991	1992	1993	1994	1995	1996	1997	1998	1999	2000	2001	2002	2003	2004	2005	2006	2007	2008	2009	2010	2011	2012	2013	2014	2015	2016	2017	2018	2019	2020	2021	2022	2023	2024	2025	2026	2027	2028	2029	2030	2031	2032	2033	2034	2035	2036	2037	2038	2039	2040	2041	2042	2043	2044	2045	2046	2047	2048	2049	2050	2051	2052	2053	2054	2055	2056	2057	2058	2059	2060	2061	2062	2063	2064	2065	2066	2067	2068	2069	2070	2071	2072	2073	2074	2075	2076	2077	2078	2079	2080	2081	2082	2083	2084	2085	2086	2087	2088	2089	2090	2091	2092	2093	2094	2095	2096	2097	2098	2099	2100	

[illegible][illegible]

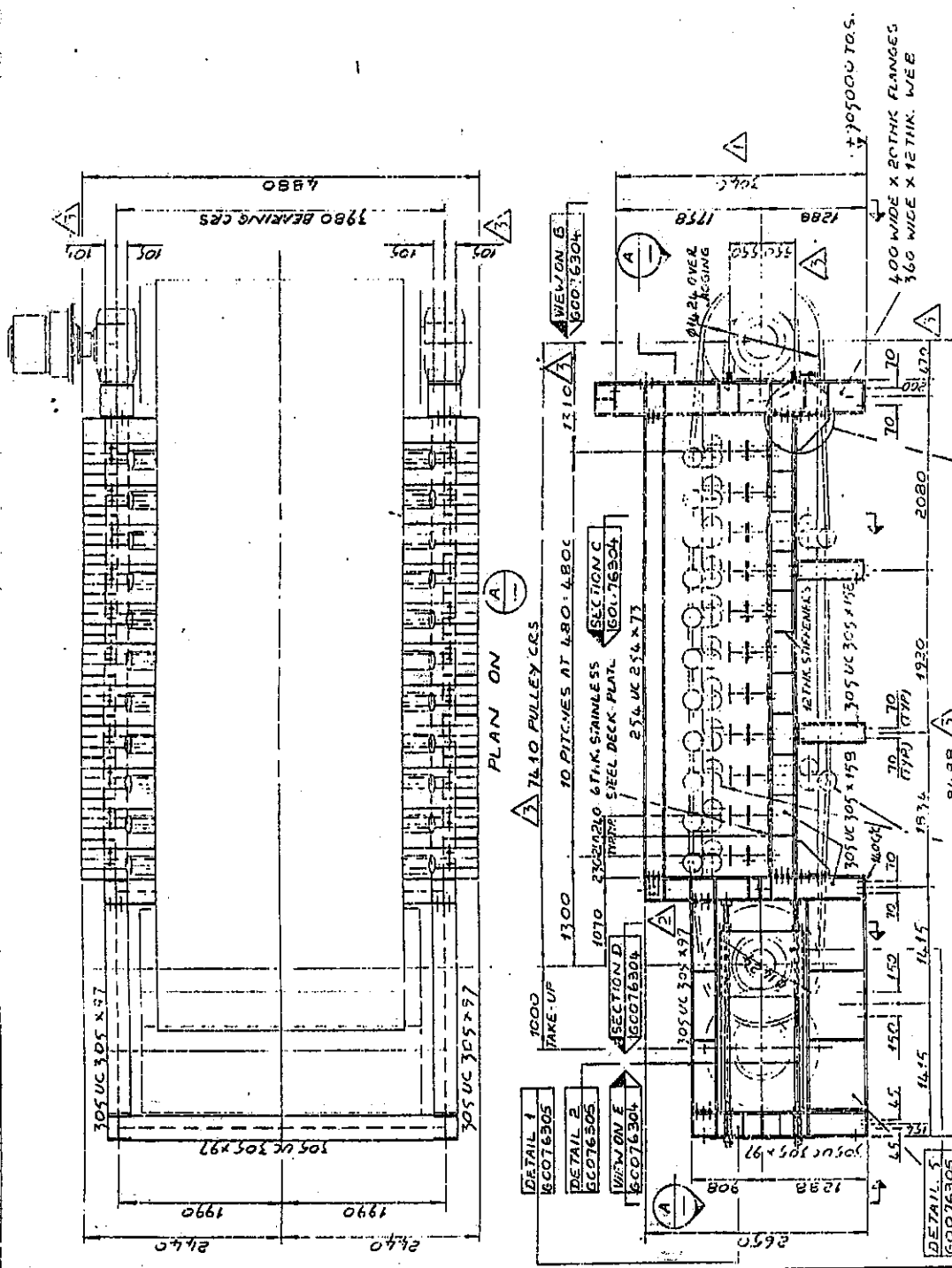
# STEELWORK GENERAL NOTES

1. STEELWORK TO BE OF BOLTED CONSTRUCTION U.O.S.
2. WELDS REQUIRED TO BE OF WELDED CONSTRUCTION, EXCEPT CHANNELS, PLATES, WELLS, U.O.S.
3. STEELWORK TO BE TO BS-48.
4. FABRICATION AND ASSEMBLY TOLERANCES TO BE AS PROJECT SPECIFICATION.
5. STEELWORK TO BE PREPARED AND PAINTED TO PROJECT SPECIFICATION U.O.S.
6. ALL HOLES TO BE 22.4 FOR M20 BOLTS U.O.S.
7. LENGTH OF SCOTED HOLES, DIMENSIONED ON DRAWING TO BE TOTAL LENGTH OF SCOT.
8. SECTION BOLTS, NUTS AND WASHERS TO BE PLACED IN NESSAN BAYS AND LABELED CLEARLY WITH THE ASSEMBLY MARK NUMBERS.
9. FABRICATOR TO SUPPLY T.O. PRINTS OF ALL SHOP DETAIL DRAWINGS WITH ERECTION MARKS TO BE CLEAR FOR APPROVAL PRIOR TO FABRICATION.

ITEM	DESCRIPTION	QTY	UNIT	PRICE	TOTAL
1	STEELWORK	1	TON	12.50	12.50
2	WELDS	1	TON	12.50	12.50
3	PAINT	1	TON	12.50	12.50
4	TRANSPORT	1	TON	12.50	12.50
5	ERECTOR	1	TON	12.50	12.50
6	WELDER	1	TON	12.50	12.50
7	PAINTER	1	TON	12.50	12.50
8	DRIVER	1	TON	12.50	12.50
9	LABOURER	1	TON	12.50	12.50
10	OVERHEAD CRANE	1	TON	12.50	12.50
11	WINDMILL	1	TON	12.50	12.50
12	WINDMILL	1	TON	12.50	12.50
13	WINDMILL	1	TON	12.50	12.50
14	WINDMILL	1	TON	12.50	12.50
15	WINDMILL	1	TON	12.50	12.50
16	WINDMILL	1	TON	12.50	12.50
17	WINDMILL	1	TON	12.50	12.50
18	WINDMILL	1	TON	12.50	12.50
19	WINDMILL	1	TON	12.50	12.50
20	WINDMILL	1	TON	12.50	12.50

Wetson, Edwards, Ltd. Spuy en val Linde (Ing.)

ITEM	DESCRIPTION	QTY	UNIT	PRICE	TOTAL
1	STEELWORK	1	TON	12.50	12.50
2	WELDS	1	TON	12.50	12.50
3	PAINT	1	TON	12.50	12.50
4	TRANSPORT	1	TON	12.50	12.50
5	ERECTOR	1	TON	12.50	12.50
6	WELDER	1	TON	12.50	12.50
7	PAINTER	1	TON	12.50	12.50
8	DRIVER	1	TON	12.50	12.50
9	LABOURER	1	TON	12.50	12.50
10	OVERHEAD CRANE	1	TON	12.50	12.50
11	WINDMILL	1	TON	12.50	12.50
12	WINDMILL	1	TON	12.50	12.50
13	WINDMILL	1	TON	12.50	12.50
14	WINDMILL	1	TON	12.50	12.50
15	WINDMILL	1	TON	12.50	12.50
16	WINDMILL	1	TON	12.50	12.50
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19	WINDMILL	1	TON	12.50	12.50
20	WINDMILL	1	TON	12.50	12.50



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4	TRANSPORT	1	TON	12.50	12.50
5	ERECTOR	1	TON	12.50	12.50
6	WELDER	1	TON	12.50	12.50
7	PAINTER	1	TON	12.50	12.50
8	DRIVER	1	TON	12.50	12.50
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12	WINDMILL	1	TON	12.50	12.50
13	WINDMILL	1	TON	12.50	12.50
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15	WINDMILL	1	TON	12.50	12.50
16	WINDMILL	1	TON	12.50	12.50
17	WINDMILL	1	TON	12.50	12.50
18	WINDMILL	1	TON	12.50	12.50
19	WINDMILL	1	TON	12.50	12.50
20	WINDMILL	1	TON	12.50	12.50